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## *Effect of confinement on local heat transfer distribution in air jet*

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## **Abstract:**

Impinging jets are used in a variety of industrial applications. The intensity move characteristics of impinging jets have been studied extensively in the literature. The authors discuss the impact of the impinging jet on the surface of strong surfaces. They also discuss possible knowledge gaps in the theory of impingement jets. The stagnation point has the greatest wall static pressure coefficient of all the configurations studied, while the streamwise direction has the lowest..An acceleration down the plate might account for this pattern..At an  $x/D_h$  ratio of 1.5, the wall jet zone is established..R.K. Brahma (1992) assessed the liquid stream and intensity move qualities at the stagnation point initiated by the fly's effect on the level surface by changing the separation from the spout to the fly and the Reynolds number..The outcomes were dissected and contrasted with those delivered by producing two-layered jets on a level surface, with the outcomes being expressed as far as the speed profile at the spout exit. Experimental research into the enhancement of heat transfer from a flat surface by normal impingement of a slot air jet due to removable confinement plates on an axis-symmetric nozzle is conducted. Using a single slot with the following parameters: aspect ratio = 25, Reynolds number = 10,000, and  $Z/D_h = (0.25) (0, 8)$ . With different confinement lengths (L) and diameters (DH), The Nussle number for the heated target plate is given in two forms: a local value and an average value.

## **Keywords:**

Air jet, Nussle Number, Static Region, Heat Transfer, Impingement, Confined Slot

### 1. Introduction:

Impinging jets are utilized in a large number of ventures since they increment the convective cooling, heating, and drying coefficient. Chilling hot parts in gas turbine motors, de-icing airplane frameworks, PCs, and electronic instruments, tempering glass plates, drying fabrics, annealing metal sheets, and making paper products are only some of the other applications. The intensity move characteristics and liquid progression of an impinging plane are impacted by numerous components, for example, the spout to-plate distance ( $Z/Dh$ ), the spout structure, and the Reynolds number. A jet whose radial spread is contained by a confinement plate is said to have a restricted flow field boundary. Since confined geometry has important industrial applications, it has been studied extensively in the literature. Cool air bled from the compressor is often used for cooling the gas turbine blade.

### 2. Structure of impinging jet:

A system having unrestricted jet exiting after impingement on a surface is called an unconfined jet impingement system. In Fig. 1, we notice the stream field brought about by a fly impinging on a symmetrical plate. The stream designs of an impinging axi-symmetric fly might be separated into three separate districts. Free jet zone (1) this is the zone of stagnant flow. Area 3: The Wall Jets

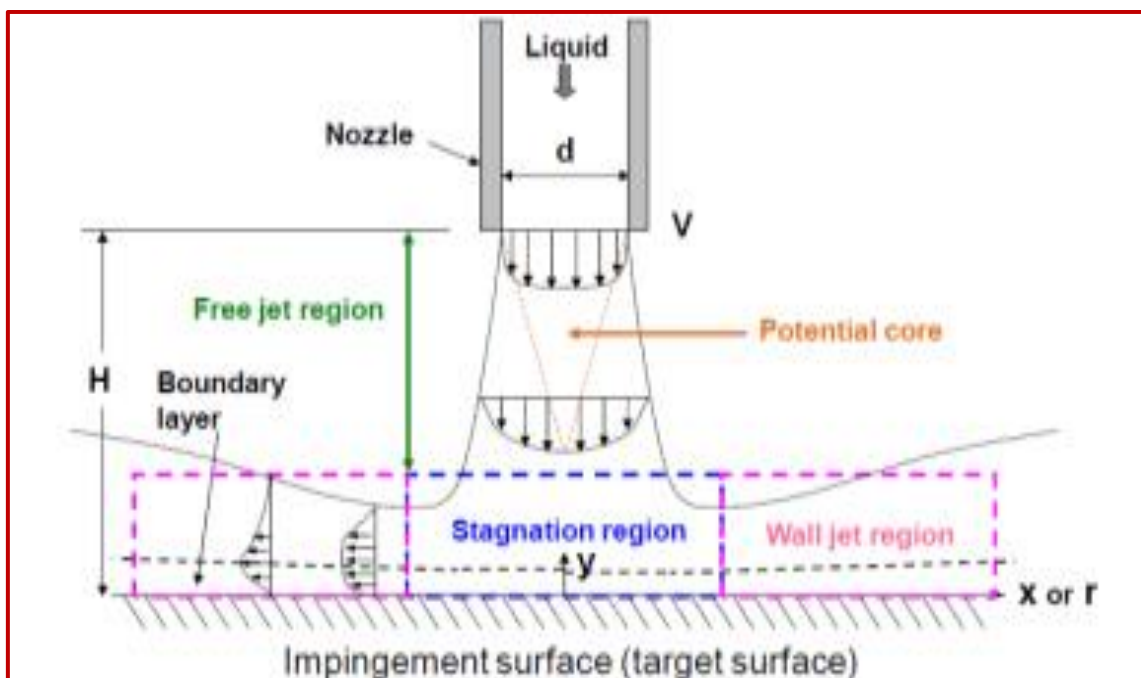


Figure. 1: Flow Regions for an Impinging Jet

From a distance of 1.2. Spout breadths, the impinging jets arrive at the objective plate surface as a free fly. The jet's momentum is being transformed into static pressure, and the flow is slowing down as a result. The stagnation zone is where the Boundary layer develops, and its thickness is constant throughout a region around 1.1 times the nozzle's diameter. Within the region of stagnation flow, the axial velocity decreases and the axial velocity becomes the tangential velocity. The exit Reynolds number is directly related to the boundary layer thickness. As a result of exchanging energy with the still environment and rubbing against the wall, the accelerated tangential flow modifies into a slowed wall jet stream. The speed fluctuations of the free jet are tracked as they propagate along the wall jet zone. In any case, the extension of the stream toward the wall region is reliant upon choppiness in the fly before impingement. The intensity move rate is viewed as higher in the wall fly area contrasted with the stream wise bearing across the plate.

### **3. Literature outline:**

Experiments have been undertaken to learn more about the structure of the submerged jet and other jet areas, in addition to the regional dispersion of the heat flux impinging on the surface. Underneath, we discuss possible knowledge gaps with regards to the various geometries of strong surfaces. Robert Gardon and J.Cahit Akfirat (1965) concentrated on the impact of intensity move boundaries on the choppiness disseminations in lowered jets brought about by impinging jets. One of a kind to opening planes, the spiral circulation of neighborhood heat move coefficients shows a greatest close to the stagnation point, with extra pinnacles, contingent upon the distance between the spout and the plate. At radii in excess of six spout distances across from the stagnation point, K. concentrated on tempestuous planes with Reynolds numbers past the scope of 5000-124,000. Jambunathan et al. in 1992 for their work on a single circular jet of heat transfer data. Higher speeds may be achieved by jets emitted from square-cornered orifices. It was observed that the temperature of the ambient air was not the same as the air leaving the nozzle, and that the jets' shape changed from elliptical and stream-like to circular. Experiments on slot jets on a submerged flat plate were conducted by V. Narayanan et al. (2004). Having a hydraulic diameter of 0.5 for the prospective core area and a diameter of 3.5 for the transitional zone. The intensity move coefficient is seen to have a most extreme in the impingement zone and a step by step diminishing pattern in the wall-limited region. To figure out what happens when a restricted air fly encroaches on a level plate at a higher Reynolds number, E.Baydar and Y. Ozmen (2005) directed tests and dissected the

discoveries mathematically. They came at the conclusion that the Reynolds number was somewhere between 30000 and 50000  $z/d$  for speeds between 0.2 and 6.0. Because of the impingement plate, the stream's speed is slowed down. The sub-barometrical region becomes noticeable with  $z/d$  values up to 2. As the spout's exit is farther from the plate, the sub atmospheric pressure spreads outward in a circular pattern. Heat transfer coefficient, turbulence intensity, and atmospheric pressure were all shown to be related. M. Nirmalkumar, Vadiraj Katti, and S.V. Prabhu (2011) performed tests to decide the intensity move conduct of a space fly in the stagnation zone ( $0 < x/b < 2$ ), the change region ( $2 < x/b < 5$ ), and the wall fly locale ( $x > 5$ ). For a given worth of  $z/b$ , an expansion in the Reynolds number in the stream wise heading brings about a more noteworthy intensity move coefficient. The optional pinnacle of an opening plane isn't noticeable at low Reynolds numbers and huge  $z/b$  s, yet it turns out to be promptly evident at a most extreme Reynolds number of 12,000. Vadiraj V. Katti, Adimurthy.M, and Ashwini M. Tamagond delivered their work in 2014. Tentatively we looked at the varieties in the wall's static strain coefficient that came about because of an opening air stream impinging on a smooth and an unpleasant surface. With a continuous stream to plate distance and a flat surface, it is shown that the wall static strain coefficient is free of Reynolds number in the range of 5000–20000. The co-efficient decreases as the distance between the stream and the plate grows because the impact affects the still air around it. The stagnation point has the greatest wall static pressure coefficient of all the configurations studied, while the streamwise direction has the lowest. An acceleration down the plate might account for this pattern. At an  $x/D_h$  ratio of 1.5, the wall jet zone is established. R.K. Brahma (1992) assessed the liquid stream and intensity move qualities at the stagnation point initiated by the fly's effect on the level surface by changing the separation from the spout to the fly and the Reynolds number. The outcomes were dissected and contrasted with those delivered by producing two-layered jets on a level surface, with the outcomes being expressed as far as the speed profile at the spout exit.

#### 4. Experimental set up:

Fig. 2. Is a schematic depicting the different parts of the experimental setup? Measurements in the field of heat transfer research. The volume of air created by a blower might be determined utilizing an aligned opening meter. Stream rate is controlled utilizing a Venturimeter or an opening meter. To keep a steady wind stream at the spout's outlet, the air is coordinated into the plenum chamber through a diffuser and two lattices. The diffuser installed ahead of the plenum ensures a uniform velocity profile. The nozzle is 45 mm in height and is fashioned from a 4 mm broad sheet of acrylic. At a 25-degree angle from the nozzle, the aspect ratio is preserved. A

Thermocouple (ChromelAlumel - K-type) is used to gauge the temperature at the jet's outlet. In order to determine the thermocouple's output, a millivolt meter is used. In order to handle a broad variety of jet-to-plate distances, the objective plate is kept on a 2-layered cross table and might be effortlessly moved. A fan is utilized in this task to move air around. It has a greatest wind stream pace of 3.5 m<sup>3</sup>/min and a load of 1.7kg. The greatest force of the blower is 600 watts. Orifice meters and venturimeters, shown in Fig. 2, are flow devices used to measure the volume of air passing through the test apparatus. Orifices are copper-coated M.S. plates with a circular hole in the center and a sharp rim. Its diameter is 10.3 millimeters. The flow line pipe that the orifice meter is attached to has a diameter of 26.2 mm. To get the same Reynolds number as air, water is utilized to calibrate orifice meters. Assuming the flow is incompressible across that distance, this is correct. The release coefficient is estimated to be 0.7. The Venturimeter is introduced in a smooth out lined up with the whole meter, producing a turbulent stream character and therefore the required flow rate. Produced using copper-covered M.S. plate, its vast throat is very limited. The venturimeter is placed perpendicular to the orifice meter to provide a high flow rate at a high Reynolds number. This study focuses on the Jet's dynamics at plate distances ( $Z/D_h$ ) of 0.25-0.50, 1.0-2.0, 4.0-6.0, and 8.0-8.0. At the nozzle's outflow, a slot is carved into a rectangular acrylic sheet that serves as the confinement plate. For the purpose of studying heat transmission, a target plate (155 mm x 60 mm x 0.06 mm - stainless steel foil) is stretched and secured between copper bus bar. The coil is held securely by bus bars that enclose about 5 mm of it on both sides. As demonstrated in fig. 4.1, the target plate assembly maintains a consistent heat flow thanks to the thin foil surface. A controlled DC power source is used to heat the target plate. To reduce heat loss via its back, heated components are coated with "Matt completion Asian" paint, with an emissivity of 0.92.

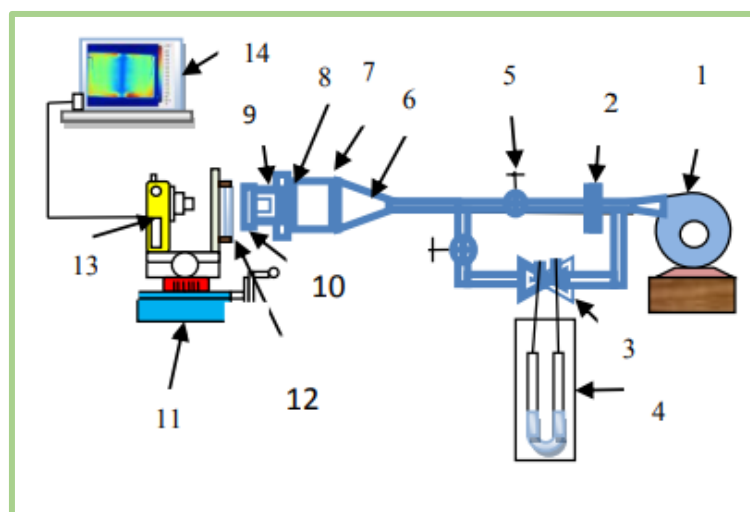


Figure. 2: Experimental set up for Heat transfer

1) Air blower 2) Orifice meter 3) Venturimeter 4) Utube manometer 5) Control valves 6) Diffuser 7) Plenum chamber 8) Flow stream 9) Slot Nozzle 10) Confinement plate 11) Traverse table 12) Target plate 13) I R Camera 14) I R Image.

## 5. Methodology:

Before the air reaches the diffuser, it is monitored using a Venturimeter or orifice meter. The needed Reynolds number of 10000 is achieved by regulating the air flow using a gate valve. Slot jets may have a confinement ratio anything from 6.8 to 27.23. The slit in the confinement plate is 60 mm by 12 mm by 10 mm thick, and it is maintained in a perpendicular position to the target plate. Slot jet to target plate division within permissible aperture limits, as measured orthogonally by  $Z/D_h = 0.25-0.8$ . Target plates are painted with black paint so that the images captured by sensitive I R cameras may be seen clearly. The included SMART VIEW software performs an analysis of the thermal pictures acquired.

## 6. Data reduction:

For given area of exit and inlet with the variation of limb height in manometer & density of water and air with constant co-efficient of discharge the Flow rate calculated as.

$$Q = C_d \frac{A_i A_o}{\sqrt{A_i^2 - A_o^2}} \sqrt{2g \left[ \frac{\rho_w}{\rho_{air}} - 1 \right] h_{mano}} \dots m^3/s$$

For rectangular shape of size of length and breadth the Hydraulic diameter is found to be as

$$D_h = \frac{4 \times \text{Area}}{2 \times \text{perimeter}} = \frac{(2 \times a \times b)}{(a+b)} \text{ m}$$

For perfect voltage and current with the area and ambient temperature of medium the heat transfer co-efficient is estimated as

$$h = \frac{V \times I}{A(T_w - T_\infty)} \text{ W/m}^2\text{K}$$

For given hydraulic diameter, velocity and density of medium with kinematic viscosity the Reynolds number is found to be as

$$Re = \frac{\rho V_j D_h}{\mu}$$

For given heat transfer coefficient with hydraulic diameter and thermal conductivity of material the Nusselt Number found as

$$Nu = \frac{h D_h}{k}$$

## 7. Results & discussion:

Thought is given to the effect of control proportion and stream to-target distance on the appropriation of intensity move coefficients. The measurement of the fly changed from 0.6 to 2 mm, and the separation from the stream to the objective plate was somewhere in the range of 0.5 and 10. When the aircraft reached the laminar zone, the Reynolds number increased from 268 to 1000. According to Z.Q. Lou et al. (2005), the laminar limit layer characteristics are  $W = 2$  mm,  $H = 5$  mm, and  $Re = 268.4$ . This improvement in laminar flow performance is just 1%. This is why we focused on creating a turbulent flow, denoted by the value  $Re = 10000$ . This knowledge will be helpful for the  $Re = 10,000$  constrained slot air jet. a) No Restraints Jet For an unconfined jet with  $Re = 10000$ , the dispersal  $Z/D_h$  might be anywhere from 0.25 to 8.0. An objective plate's neighborhood Nusselt number conveyance along the  $Z/D_h$  hub is found in Fig. 3. At the place of stagnation, The Nusselt number for  $Z/D_h = 0.25$  in the neighborhood is around 1.5 times that of  $Z/D_h = 8.0$ . Move coefficient assumes a pivotal part in the computation of the Nusselt number. The Nusselt number increases significantly at the stagnation point and in the downstream zone when  $Z/D_h$  is reduced from 8.0 to 0.25. The change in the intensity move coefficient in the wall stream zone is harsh toward the worth of  $Z$  when  $Z/D_h$  is bigger than 1. When  $Z/D_h$  is decreased, the Nusselt number at the jet's core rises considerably.

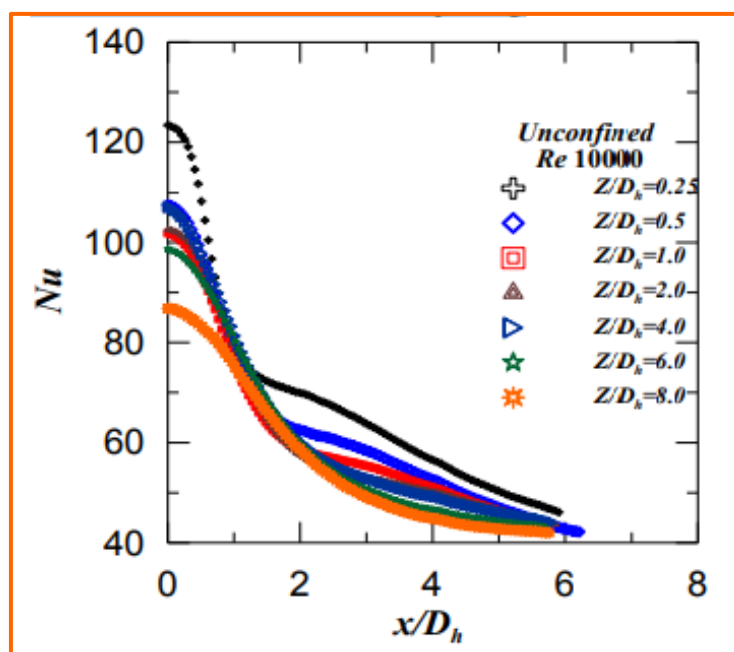
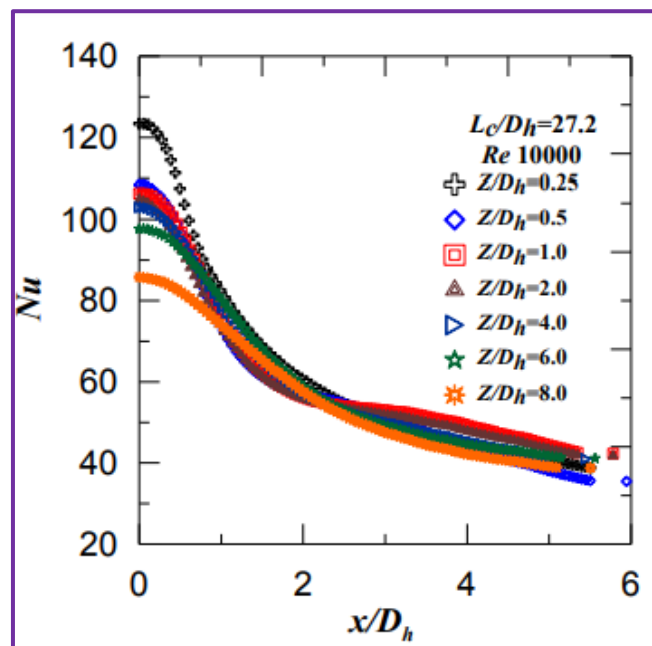
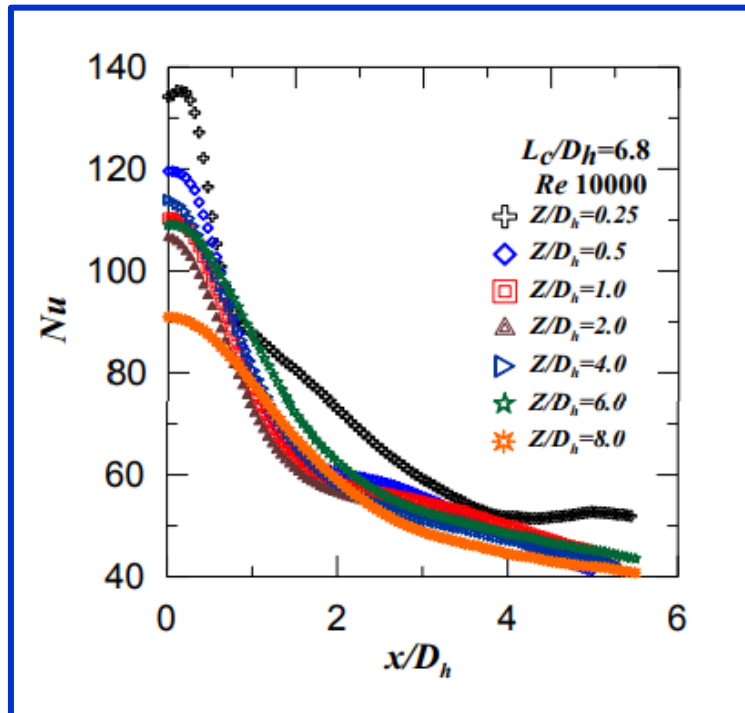


Figure.3: the effect of control proportion and stream

Distance from nozzle to target and its effect: The scattering  $Z/D_h$  from the stream to the objective reaches from 0.25 to 8.0 and the  $L_c/D_h$  goes from 6.8 to 27.23 for  $Re = 10000$ . In Fig. 4, we see the neighborhood Nusselt number conveyed as a component of  $Z/D_h$  along the



objective plate. The neighboring Nusselt number is about 1.5 times larger for  $Z/D_h = 0.25$  than for  $Z/D_h = 8$  at the stagnation point. The Nusselt number is estimated in large part by the heat move coefficient. The Nusselt number increases significantly at the stagnation point and in the downstream zone when the percentage of  $Z/D_h$  is reduced from 8.0 to 0.25. The change in the intensity move coefficient in the wall fly zone is coldhearted toward the worth of  $Z$  when  $Z/D_h$  is bigger than 1. When  $Z/D_h$  is decreased, the Nusselt number at the jet's core rises considerably.



Confined slot jets of sizes  $L_c/D_h = 6.8$  and  $L_c/D_h = 27.23$  at  $Re = 10000$ : Effect of  $Z/D_h$  ratio on local heat transfer distribution Relative confinement's impact: In this investigation, we employ

a wide range of values for the confinement ratio ( $L_c/D_h$ ) while keeping the Reynolds Number ( $Re$ ) at 10000. As can be seen in Fig. 5, the heat transfer coefficient is around 0.25 for a broad range of  $Z/D_h$  values. As everything reach a standstill, the Nusslet number of the surface increases as  $x/D_h$  goes down, whereas the Nusslet number of the wall in the jet zone goes down as  $x/D_h$  goes up. The jet's core becomes more defined as  $x/D_h$  decreases. At the point when the repression proportion is 6.8 and the intensity move rate in the stagnation district is ideal, as it is when  $Z/D_h = 0.25$  and  $L_c/D_h = 6.8$ , the thermal performance is ideal. According to Table I, at  $Re = 10000$ , a  $Z/D_h = 0.25$  gives a +8.76% boost in thermal efficiency when the confinement ratio  $L_c/D_h$  is 6.8, whereas  $L_c/D_h = 17.0$  and  $L_c/D_h = 20.6$  have great preferences but lower efficiency.  $Nu_o$  is unaffected by the ratio of  $L_c/D_h$  between 13.6 and 27.23, and the ratios of 10.2 and 23.8, which lower the Nusselt number compared to an unconfined jet are should be avoided.

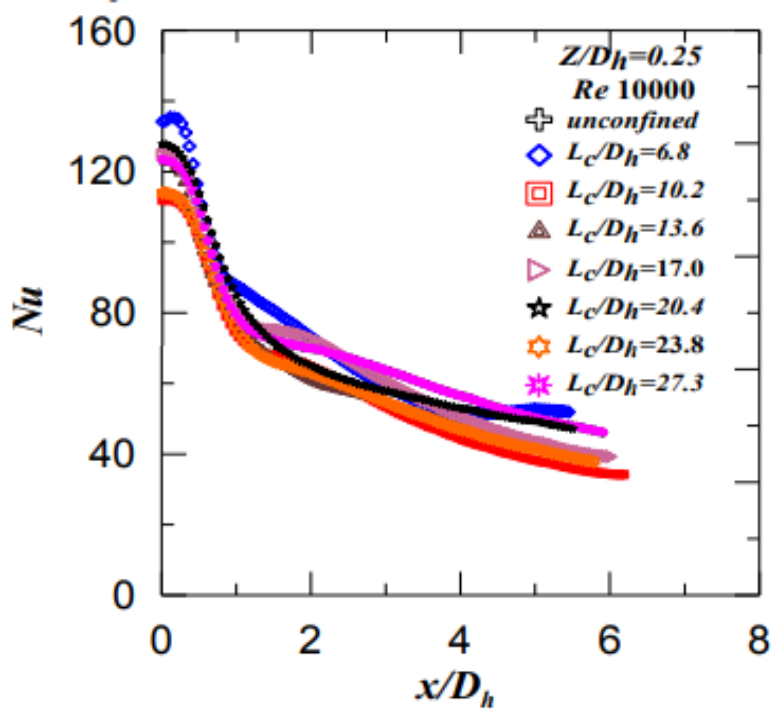


Figure. 4: Effect of the  $L_c/D_h$  ration on Local heat transfer Distribution for Confined Slot air Jet for  $Re$  10000 at  $Z/D_h$  at 0.25.

Table.1: Details for influence of confinement

Unconfined Slot Air Jet $Nu_o = 123.41$ at $Z/D_h = 0.25$ for $Re = 10000$		
$L_c/D_h$	$Nu_o$	Percentage of $Nu_o$ on Confined Slot Air Jet
6.8	134.2	+ 08.7 % Better preferences

10.2	111.8	- 09.3 % Not preferred
13.6	122.7	- 00.5 % No influence
17.0	124.8	+ 01.1 % Good preferences
20.6	127.0	+ 03.6 % Good preferences
23.8	114.2	- 07.0 % Not preferred
27.2	123.7	- 00.0 % No influence

The proposition of confinement has values between 6.8 and 27.23. We held the other variables at  $Re = 10000$ . As may be observed in Fig. 6. That the surface Nusslet number increases as  $x/D_h$  gets closer to the stagnation point, and that it reduces as  $x/D_h$  goes up in the wall jet area. This holds true for a wide range of confinement ratios, but is most pronounced when  $Z/D_h = 0.5$ . The potential core area becomes more defined as  $x/D_h$  decreases. Here, the core heat transfer rate is maximized at 17.0&6.8 with a confinement ratio of  $L_c/D_h$ . Therefore, the  $L_c/D_h = 6.8$  provides superior thermal performance at the optimal heat transfer rate of  $Z/D_h = 0.5$ . The highest thermal performance is achieved with a heat transfer coefficient of 17.0 at  $Z/D_h = 0.5$  and unconfined conditions in the wall jet zone.

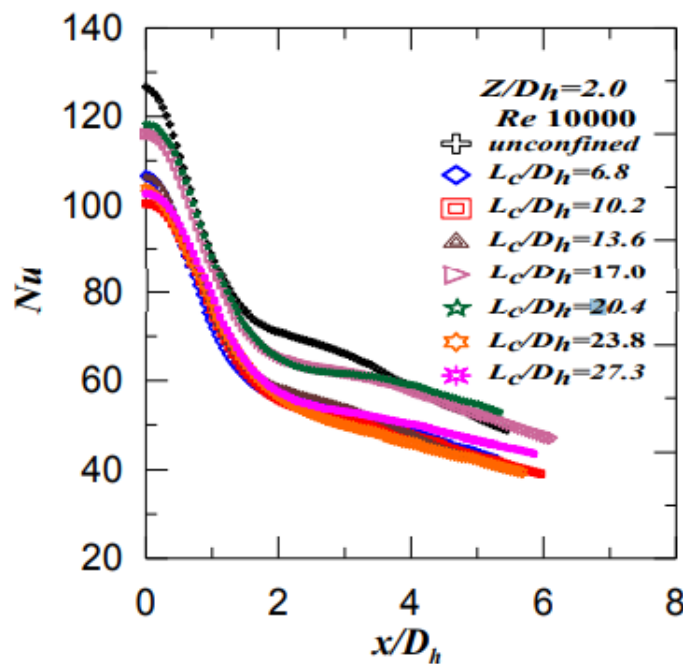


Figure.8: Effect of the  $L_c/D_h$  ratio on Local heat transfer distribution for Confined Slot air Jet for  $Re 10000$  at  $Z/D_h$  at 2.0.

Based on the data in Table II, we can deduce that a confinement ratio  $L_c/D_h$  of 20.6 provides +11.47% improved thermal efficiency for the given  $Z/D_h = 0.5$  at  $Re = 10000$ , whereas  $L_c/D_h$  values of 6.8, 13.6, 17.0, and 27.2 have excellent preferences but less efficiency than  $L_c/D_h = 20.6$ .  $Nu_o$  is unaffected by an  $L_c/D_h$  between 13.6 and 27.23. Both 10.2 and 23.8 for  $L_c/D_h$  are inferior to the unconfined jet in terms of Nusselt number.

Using the information in Table IV, we can deduce that a confinement ratio of 20.6 provides +15.30% greater thermal efficiency than a ratio of 6.8, 13.6, 23.8, or 27.2 for a given  $Z/D_h = 2.0$  at  $Re = 10000$ . Nusselt number decreases when comparing the confined jet to the unconfined jet, hence an  $L_c/D_h$  of 10.2 is not optimal.

*Table. IV: Details for influence of confinement*

Unconfined slot air jet $Nu_o = 102.55$ at $Z/D_h = 2.0$ for $Re = 10000$		
$L_c/D_h$	$Nu_o$	Percentage of $Nu_o$ on Confined Slot Air Jet
6.8	106.5	+ 0.390 % Good preferences
10.2	100.2	- 02.20 % Not preferred
13.6	106.1	+ 03.40 % Good preferences
17.0	116.0	+ 13.10 % Good preferences
20.6	118.2	+ 15.30 % Good preferences
23.8	103.7	+ 01.14 % Good preferences
27.2	104.9	+ 02.33 % Good preferences

## 8. Conclusion:

The heat transfer coefficients' spatial distribution in a flat system we undertake an experimental investigation of the impingement of a limited slot air jet at  $Re = 10000$ , with nozzle slot jet to plate spacings ranging from  $Z/D_h = 0.25$  to 8.0. These theories are strengthened by the findings of this study. At a Reynolds number of 10,000, it is found that the intensity move dissemination and the Nusselt number of a restricted and an unconfined opening air fly are indistinguishable. At the stagnation point, where  $L_c/D_h = 0.0-27.23$  is determined for both unconfined and

confined flows, the Nusselt number increases continuously. In both the unconfined and confined cases, heat transmission is sharpest in the core jet area. Higher jet-to-plate separation has little effect on heat transmission in either an unconfined or confined setting. For both free-flowing and restricted slot air jets, the wall jet zone is cooler than the core -region. The best preference for all  $Z/D_h$  values may be achieved with a confinement ratio of  $L_c/D_h = 6.8$ .

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